Simulation of two phase flow using a modified ACLS method

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Zalesak dísk

vortex-in-a-box

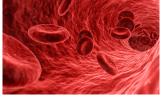
3D FHIT of liquid-gas flow

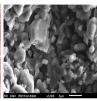
Conclusions

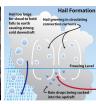
Multiphase flows

General introduction

Two-phase gas-liquid turbulent flows featuring phase changes are encountered in many natural and industrial processes







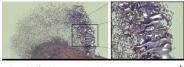
- = Effectiveness depends on many parameters
 - Volume and residence time of discrete phase, bubble rise velocity, bubble size or bubble size distribution, and bubble deformability.
- Numerical simulations could be of significant use if adapted models and methods are carefully developed

Modeling two-phase flows is challenging

- Discontinuities in density across the interface
- Díscrete conservation of:
 - mass of each fluid
 - >>> total momentum
 - kínetíc energy
- Dynamic creation of interfaces and complex topological changes
- Accurate modeling of surface tension effects

40% of mass is lost ©

Drop deformation in shearing flow a



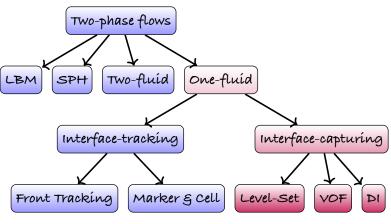
Liquid jet in a swirling gas crossflow b

a Enright, D. P. (2002). PhD Thesis. stanford university.

^bPrakash, S. R., et al. (2019). Atomization & Sprays.

Classification of Methods

Numerical methods employed for the description of the dispersed phase topology

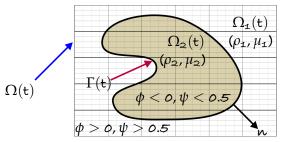


LS is the state-of-art method for incompressible flows 1

 $^{^{1}}$ Soligo G., Alessío R., and Alfredo S. (2021). Journal of Fluids Engineering.

Model problem

 $ightharpoonup \Omega \in \mathbb{R}^3$ a bounded domain such that $\overline{\Omega} = \overline{\Omega_{\mathtt{I}}(\mathsf{t})} \cup \overline{\Omega_{\mathtt{Q}}(\mathsf{t})}$ and $\Omega_{\mathtt{I}} \cap \Omega_{\mathtt{Q}} = \emptyset$ and $\Gamma(\mathsf{t}) = \partial \Omega_{\mathtt{I}}(\mathsf{t}) \cup \partial \Omega_{\mathtt{Q}}(\mathsf{t})$ is the interface between two fluids.



⇒ Immíscíble incompressible two-fluid system

$$\begin{split} \nabla \cdot \mathbf{u} &= o, \frac{\partial \mathbf{u}}{\partial \mathbf{t}} + \mathbf{u} \cdot \nabla \mathbf{u} = \frac{\mathbf{1}}{\text{Re}} \nabla \cdot \left(\mu (\nabla \mathbf{u} + \nabla \mathbf{u}^{\mathsf{T}}) \right) - \nabla \mathbf{p} + \frac{\mathbf{1}}{\text{Fr}} \mathbf{g} \end{split}$$
 with $[\mathbf{p}]_{\Gamma} = \frac{\mathbf{1}}{\text{We}} \kappa + \frac{2}{\text{Re}} [\mu]_{\Gamma} \mathbf{n}^{\mathsf{T}} \cdot \nabla \mathbf{u} \cdot \mathbf{n}$

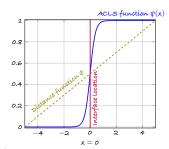
Level set method for two-fluid flows

- \Rightarrow The interface is define as $\Gamma(\mathsf{t}) = \{\mathsf{x} \in \Omega; \phi(\mathsf{x},\mathsf{t}) = \mathsf{o}\}$
- The interface movement is captured by solving the level-set equation:

$$\frac{\partial \phi}{\partial t} + \mathbf{u} \cdot \nabla \phi = o,$$

The Accurate Conservative Level Set (ACLS) method uses

$$\psi(x,t) = \frac{1}{2} \left(\tanh \left(\frac{\phi(x,t)}{2\epsilon} \right) + 1 \right)$$



where the interface location is the $\psi(\mathsf{x}, o) = o.5$ isosurface and

$$\frac{\partial \psi}{\partial t} + \nabla \cdot (\psi u) = o.$$

Level set method for two-fluid flows

- $\Rightarrow \phi$ does not maintain the property $|
 abla \phi| = \mathbf{1}$ during transport.
- In the classical ACLS method, a relaxation step is added by solving in pseudo-time

$$\frac{\partial \psi}{\partial \tau} + \nabla \cdot (\psi(\mathbf{1} - \psi)\mathbf{n}) = \nabla \cdot (\epsilon \left(\nabla \psi \cdot \mathbf{n} \right) \mathbf{n})$$

 \Rightarrow The enhanced ACLS method, the re-initialization process is²

$$rac{\partial \psi}{\partial au} =
abla \cdot \left[rac{ exttt{1}}{4 \cosh^2 \left(rac{\phi_{ exttt{MAP}}}{2 arepsilon}
ight)} \left(
abla \phi_{ exttt{MAP}} \cdot exttt{n}_{ exttt{FMM}} - exttt{n}_{ exttt{FMM}} \cdot exttt{n}_{ exttt{FMM}}
ight) exttt{n}_{ exttt{FMM}}
ight]$$

where $\phi_{\text{map}} = \epsilon \log \left(\frac{\psi}{\imath - \psi} \right)$ and n_{FMM} is obtained from a Fast Marching Method (FMM) according to $n_{\text{FMM}} = \nabla \phi_{\text{FMM}}$

 $^{^{2}}$ Desjardins O., Vincent M., and Heinz P. (2018). Journal of computational physics.

Some Numerical details

- ightharpoonup TZEM is a low-Mach number code for the DNS and LES of reacting two-phase flows.
- Projection method based on fractional time steps developed by Chorin ³ and improved by Kim § Moin ⁴.
 - Fourth-order central scheme is used for the spatial integration
 - Third-order accurate semi-implicit Crank-Nicolson scheme is employed for time integration.
- Poison equation is solved using the Livermore's Hypre library with the PCG (pre-conditioned conjugate gradient) method 5.



¹ Chorin, A. J. (1968). Mathematics of computation.

²Kim, J., & Moin, P. (1985). Journal of computational physics.

³ Falgout, R. D., and Ulrike M. Y. (2002). Computational Science – ICCS 2002.

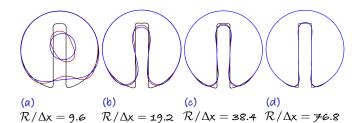
Numerical results - Zalesak dísk

we consider a domain of unit size with the slotted disk with a constant velocity field defined by



$$\begin{cases} u_1 = -2\pi \cos(x_2 - 0.5) \\ u_2 = 2\pi \sin(x_1 - 0.5) \end{cases}$$





The red and blue the solutions after one and two full revolutions.

Numerical results - Vortex-in-a-box (serpentine)

The velocity field is derived from the stream function

$$\Psi(\mathbf{x_1},\mathbf{x_2},\mathbf{t}) = \pi \sin^2(\pi \mathbf{x_1}) \sin^2(\pi \mathbf{x_2}) \cos(\pi \mathbf{t}/\mathbf{T})$$



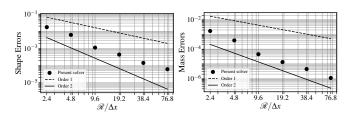
(a)
$$t = 0s$$
 (b) $t = 2s$ (c) $t = 4s$ (d) $t = 6s$ (e) $t = 8s$



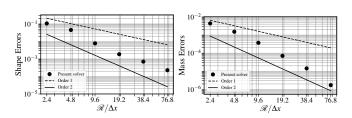
$$(f) t = 0s (g) t = 2s (h) t = 4s (i) t = 6s (j) t = 8s$$

Temporal evolution of circle deformation in a box shape (serpentine) at different times with (top row) $\mathcal{R}/\Delta x = 19.2$ and (bottom row) $\mathcal{R}/\Delta x = 76.8$.

Numerical results - Mesh error convergence



Mesh error convergence for the Zalesak's disk rotation



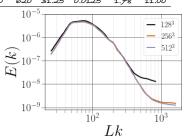
Mesh error convergence for the serpentine

Numerical results - 3D FHIT of liquid-gas flow

- ⇒ 3D cubical domain with periodic boundaries.
- 8 droplets were confined whose sum is equal to the prescribed liquid volume fraction.
- $\stackrel{ riangle}{=}$ The control-based linear forcing approach of Bassenne 6 is extended for the liquid-gas mixtures.

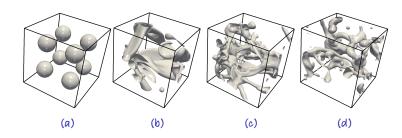
$\rho_{\ell}/\rho_{\mathfrak{g}}$	$\mu_{\ell}/\mu_{\mathfrak{g}}$	σ [N.m ⁻¹]	L [m]	ϕ_{ℓ}	$We_{\mathfrak{g}}$	$\mathcal{W}\mathfrak{e}_\ell$	Re_{ℓ}	Re_{λ}	$\mathcal{O}\mathfrak{h}_\ell$	$\Delta x/\eta_{\mathfrak{g}}$	$\lambda/\eta_{\mathfrak{g}}$
30	30	0.0135	1.5×10^{-4}	0.10	2.0	60	620	31.25	0.0125	1.78	11.00

Small-scale effects are resolved on the resolution mesh featuring 512³ grid points.



⁵Bassenne M., et al. (2016). Physics of Fluids.

Numerical results - 3D FHIT of liquid-gas flow



The temporal evolution of the liquid/carrier interface

- The interface exhibits slight wrinkling.
- The interface becomes stretched and rolled up, and undergoes complex turbulent breakup and wrinkling

Conclusions

- Major findings
 - A novel solver for the simulation of incompressible two-phase flows is introduced.
 - The numerical method employed to capture the interface is based on the ACLS technique combined with a recently developed reinitialization technique.
 - rhe solver's accuracy is assessed.
- Perspectives
 - multi-level adaptive mesh refinement method.
 - Parallel computing on unstructured grids.

Thanks for listening!

Acknowledgments



Multiphysics & HPC of UMGP